# Density and Relative Permittivity for 1-Alkanols + Dodecane at 298.15 K 

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#### Abstract

Densities and relative permittivities at a frequency of 30 kHz for the binary mixtures of 1-alkanols, $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}$ for $n=1$ to $10,+$ dodecane were measured for the mole fraction range of 1-alkanol between 0 and 0.1 at a temperature of 298.15 K. By using Debye and Frohlich equations, the apparent dipole moments ( $\mu$ ) of 1-alkanols were calculated, and the limiting values ( $\mu_{0}$ ) were determined by extrapolating to infinite dilution. The value of $\mu_{0}$ decreased with increasing hydrocarbon length of the 1 -alkanol. The present results were compared with our previous measurements in cyclohexane and heptane. Methanol had the same $\mu_{0}$ value irrespective of solvent, while $\mu_{0}$ for 1 -alkanols with $n \geq 2$ showed a lower value in dodecane than those found in cyclohexane and heptane. The excess partial molar volumes of 1-alkanols at infinite dilution decreased with increasing $n$.


## Introduction

The dipole moment ( $\mu$ ) is one of the very important properties of molecules because it is related to the molecular configuration as well as its polarity. It has been determined for many molecules by means of permittivity measurements since 1930. ${ }^{1}$ However, the values of $\mu$ accumulated in the literature show large discrepancies except the most recent ones determined by using successive dilution methods developed for solutions. ${ }^{2,3}$ Previous publications from our laboratory have reported apparent dipole moment of 1-alkanols, $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}$ for $n=1$ to 10 , in cyclohexane and heptane, and excess molar volumes ( $V_{\mathrm{m}}^{\mathrm{E}}$ ) for binary mixtures of those 1 -alkanols + cyclohexane and heptane. ${ }^{4}$ We found that the dipole moment of isolated alkanols ( $\mu_{0}$ ) determined by extrapolating to infinite dilution decreased with increasing $n$ of the 1 -alkanols. We also found a small but systematic effect on $\mu$ due to solvent. Thereby, we expected that the $\mu_{0}$ of alkanols changes with the length of hydrocarbon used for a solvent. As an extension of our previous work the apparent dipole moments $(\mu)$ of $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}$ for $n=1$ to 10 were determined in dodecane. We also measured the densities ( $\rho$ ) of those mixtures for the mole fraction $(x)$ of alkanol for $x<0.1$ at a temperature ( $T$ ) of 298.15 K .

## Experimental Section

Materials. The samples of 1-alkanol were the same as used in the previous work. ${ }^{4}$ Dodecane was Cica-special grade reagent supplied from Kanto Chemical Co. Inc. and used as received. Other liquids were purified by distillation. Their purities were tested by GLC analysis, and the mole fraction of water in the used samples was measured by Karl Fischer method. The purified liquids were kept in sealed glass ampules after replacing the atmosphere with $\mathrm{N}_{2}$ and stored in a refrigerator. The purities and the densities of the component liquids are listed in Table 1 along with literature values of refractive indices ( $n_{\mathrm{D}}$ ). The purification

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Figure 1. Excess partial molar volumes at the infinite dilution $\left(V_{2}^{\mathrm{E}, \infty}\right)$ for $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}$ at 298.15 K . Our results: O, in cyclohexane; ${ }^{4} \Delta$, in dodecane; $\square$, in heptane; ${ }^{4}$ solid line, least squares representation in cyclohexane; broken line, least squares representation in heptane; doted line, least squares representation in dodecane. Literature values: $\bullet$, in pentane; ${ }^{13,14} \bullet$, in hexane; $\boldsymbol{j}^{13,14}$ $\mathbf{\Delta}$, in hexane; ${ }^{15} \nabla$, in octane; ${ }^{13,14} \diamond$, in decane; ${ }^{13,14}+$, in hexadecane; ${ }^{14} ■$, in hexadecane. ${ }^{23}$
and the test of purity have been described in detail in the previous report. ${ }^{4}$
Measurements. The densities of $\{x 1$-alkanol $+(1-x)$ dodecane $\}$ were measured using a vibrating tube densimeter (Anton Paar, DMA-602). The temperature in the jacket of densimeter was controlled with water circulated with a temperature controller (CT-L, Sodev, Canada). It was stable within $\pm 0.0003 \mathrm{~K}$ for a period to measure several points accompanying a drift of $7 \times 10^{-4} \mathrm{~K}$ during ordinary operation period of 3 h . The resonance period showed a drift of $0.0003 \mu \mathrm{~s}$ during the operation of 3 h . This drift corresponded to a shift of $4 \times 10^{-7} \mathrm{~g} \cdot \mathrm{~cm}^{-3}$ in density. The densimeter was calibrated by using the densities of heptane, cyclohexane, toluene, benzene, and chlorobenzene. The densities of these liquids were determined by use of a $50 \mathrm{~cm}^{3}$ pycnometer with an uncertainty of $\pm 3 \times 10^{-6} \mathrm{~g} \cdot \mathrm{~cm}^{-3}$, and the vibrating tube densimeter

Table 1. Densities ( $\rho$ ) and Refractive Indices ( $n_{\mathrm{D}}$ ) at 298.15 K and Purities for the Component Liquids

| componet liquid | purity $/ \%^{a}$ | $x\left(\mathrm{H}_{2} \mathrm{O}\right) \times 10^{4 b}$ | $\rho(\mathrm{obs}) / \mathrm{g} \cdot \mathrm{cm}^{-3}$ | $\rho(\mathrm{lit}) / \mathrm{g} \cdot \mathrm{cm}^{-3}$ | $\rho(\mathrm{lit}) / \mathrm{g} \cdot \mathrm{cm}^{-3}$ |  |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: |
| dodecane | 99.96 | 2.7 | 0.745435 | $0.74518^{c}$ |  |  |
| methanol | 99.99 | 1.5 | 0.786538 | $0.78667^{d}$ | $0.78718^{h}$ |  |
| ethanol | 99.98 | 2.4 | 0.785055 | $0.78512^{d}$ | $0.78524^{h}$ |  |
| 1-propanol | 99.99 | 3.4 | 0.799564 | $0.79960^{c}$ | $0.79976^{h}$ |  |
| 1-butanol | 99.99 | 10.0 | 0.805767 | $0.80575^{c}$ | $0.80583^{h}$ |  |
| 1-pentanol | 99.80 | 7.0 | 0.810883 | $0.81119^{e}$ | $1.32661^{d}$ |  |
| 1-hexanol | 99.95 | 1.0 | 0.815275 | $0.81534^{d}$ | $1.38348^{d}$ |  |
| 1-heptanol | 99.98 | 4.7 | 0.818746 | $0.81105^{h}$ |  |  |
| 1-octanol | 99.97 | 5.5 | 0.821694 | $0.81551^{h}$ |  |  |
| 1-nonanol | 99.21 | 5.5 | 0.824263 | $0.82170^{d} e^{e}$ | $1.40790^{e}$ |  |
| 1-decanol | 99.88 | 5.5 | 0.826421 | $0.8240^{g}$ | $0.81897^{h}$ | $0.82180^{h}$ |

${ }^{a}$ Estimated by GLC analysis. ${ }^{b}$ Determined by Karl Fischer method. ${ }^{c}$ Ref 16. ${ }^{d}$ Ref $17 .{ }^{e}$ Ref 18. ${ }^{f}$ Ref 19. ${ }^{g}$ Ref 20. ${ }^{h}$ Ref 21. ${ }^{i}$ Ref 22.
Table 2. Densities ( $\rho$ ) and Excess Molar Volumes ( $V_{\mathrm{m}}^{\mathrm{E}}$ ) of (1-Alkanol + Dodecane) at 298.15 K

| $x$ | $\frac{\rho}{\mathrm{g} \cdot \mathrm{~cm}^{-3}}$ | $\frac{V_{\mathrm{m}}^{\mathrm{E}}}{\mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}}$ | $x$ | $\frac{\rho}{\mathrm{g} \cdot \mathrm{~cm}^{-3}}$ | $\frac{V_{\mathrm{m}}^{\mathrm{E}}}{\mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}}$ | $x$ | $\frac{\rho}{\mathrm{g} \cdot \mathrm{~cm}^{-3}}$ | $\frac{V_{\mathrm{m}}^{\mathrm{E}}}{\mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}}$ | $x$ | $\frac{\rho}{\mathrm{g} \cdot \mathrm{~cm}^{-3}}$ | $\frac{V_{\mathrm{m}}^{\mathrm{E}}}{\mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $x \mathrm{CH}_{3} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{3} \mathrm{H}_{7} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{4} \mathrm{H}_{9} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |
| 0.00135 | 0.745406 | 0.0078 | 0.00284 | 0.745404 | 0.0185 | 0.00273 | 0.745430 | 0.0173 | 0.00247 | 0.745450 | 0.0139 |
| 0.00185 | 0.745400 | 0.0110 | 0.00350 | 0.745397 | 0.0226 | 0.00429 | 0.745426 | 0.0269 | 0.00337 | 0.745455 | 0.0189 |
| 0.00406 | 0.745379 | 0.0224 | 0.00482 | 0.745386 | 0.0302 | 0.00700 | 0.745424 | 0.0422 | 0.00504 | 0.745466 | 0.0281 |
| 0.00925 | 0.745332 | 0.0483 | 0.00760 | 0.745363 | 0.0458 | 0.01162 | 0.745429 | 0.0659 | 0.00890 | 0.745497 | 0.0474 |
| 0.01113 | 0.745324 | 0.0548 | 0.01169 | 0.745338 | 0.0661 | 0.01810 | 0.745456 | 0.0931 | 0.01274 | 0.745535 | 0.0643 |
| 0.01828 | 0.745284 | 0.0828 | 0.01342 | 0.745329 | 0.0742 | 0.02480 | 0.745504 | 0.1152 | 0.01568 | 0.745569 | 0.0761 |
| 0.02969 | 0.745265 | 0.1136 | 0.01890 | 0.745313 | 0.0959 | 0.04304 | 0.745689 | 0.1601 | 0.02553 | 0.745703 | 0.1090 |
| 0.04640 | 0.745259 | 0.1523 | 0.02678 | 0.745305 | 0.1226 | 0.06062 | 0.745916 | 0.1901 | 0.04126 | 0.745979 | 0.1445 |
| 0.06420 | 0.745271 | 0.1882 | 0.04127 | 0.745348 | 0.1547 | 0.07866 | 0.746164 | 0.2180 | 0.06044 | 0.746372 | 0.1729 |
| 0.08321 | 0.745289 | 0.2251 | 0.06055 | 0.745432 | 0.1898 | 0.10253 | 0.746495 | 0.2572 | 0.07754 | 0.746736 | 0.1965 |
| 0.09518 | 0.745306 | 0.2467 | 0.08084 | 0.745514 | 0.2295 |  |  |  | 0.10338 | 0.747278 | 0.2391 |
|  |  |  | 0.09645 | 0.745601 | 0.2535 |  |  |  |  |  |  |
| $x \mathrm{C}_{5} \mathrm{H}_{11} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{6} \mathrm{H}_{13} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{7} \mathrm{H}_{15} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{8} \mathrm{H}_{17} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |
| 0.00199 | 0.745463 | 0.0108 | 0.00175 | 0.745477 | 0.0096 | 0.00183 | 0.745491 | 0.0096 | 0.00204 | 0.745513 | 0.0105 |
| 0.00476 | 0.745503 | 0.0250 | 0.00460 | 0.745539 | 0.0244 | 0.00384 | 0.745550 | 0.0193 | 0.00419 | 0.745594 | 0.0203 |
| 0.00753 | 0.745546 | 0.0380 | 0.00826 | 0.745625 | 0.0410 | 0.00719 | 0.745657 | 0.0335 | 0.00734 | 0.745718 | 0.0336 |
| 0.01643 | 0.745714 | 0.0721 | 0.01788 | 0.745888 | 0.0742 | 0.01509 | 0.745934 | 0.0595 | 0.01454 | 0.746026 | 0.0564 |
| 0.02691 | 0.745951 | 0.1010 | 0.02646 | 0.746157 | 0.0938 | 0.02602 | 0.746357 | 0.0845 | 0.02591 | 0.746560 | 0.0792 |
| 0.03525 | 0.746159 | 0.1186 | 0.03537 | 0.746455 | 0.1094 | 0.03537 | 0.746740 | 0.0998 | 0.03144 | 0.746830 | 0.0872 |
| 0.05055 | 0.746571 | 0.1433 | 0.04959 | 0.746947 | 0.1307 | 0.04943 | 0.747341 | 0.1174 | 0.04912 | 0.747720 | 0.1074 |
| 0.06514 | 0.746983 | 0.1632 | 0.06560 | 0.747525 | 0.1500 | 0.06486 | 0.748019 | 0.1333 | 0.06408 | 0.748489 | 0.1217 |
| 0.08115 | 0.747444 | 0.1846 | 0.07934 | 0.748030 | 0.1660 | 0.08181 | 0.748778 | 0.1492 | 0.08146 | 0.749394 | 0.1377 |
| 0.09931 | 0.747979 | 0.2082 | 0.09708 | 0.748704 | 0.1826 | 0.10235 | 0.749709 | 0.1693 | 0.10144 | 0.750468 | 0.1499 |
| $x \mathrm{C}_{9} \mathrm{H}_{19} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  | $x \mathrm{C}_{10} \mathrm{H}_{21} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |  |  |  |  |  |  |
| 0.00099 | 0.745467 | 0.0050 | 0.001264 | 0.745351 | 0.0065 |  |  |  |  |  |  |
| 0.00470 | 0.745637 | 0.0216 | 0.002235 | 0.745401 | 0.0114 |  |  |  |  |  |  |
| 0.00777 | 0.745786 | 0.0329 | 0.004620 | 0.745527 | 0.0223 |  |  |  |  |  |  |
| 0.01456 | 0.746133 | 0.0527 | 0.011828 | 0.745934 | 0.0482 |  |  |  |  |  |  |
| 0.02651 | 0.746790 | 0.0744 | 0.032299 | 0.747221 | 0.0828 |  |  |  |  |  |  |
| 0.03533 | 0.747291 | 0.0860 | 0.056688 | 0.748861 | 0.0954 |  |  |  |  |  |  |
| 0.05117 | 0.748212 | 0.1021 | 0.083338 | 0.750666 | 0.1093 |  |  |  |  |  |  |
| 0.06465 | 0.749011 | 0.1131 | 0.106910 | 0.752273 | 0.1223 |  |  |  |  |  |  |
| 0.08043 | 0.749970 | 0.1205 |  |  |  |  |  |  |  |  |  |
| 0.09832 | 0.751064 | 0.1297 |  |  |  |  |  |  |  |  |  |

Table 3. Coefficients $\left(d_{j}\right)$ and Estimated Standard Uncertainties $\left(u_{d}\right)$ Determined by Eq 7 for $\{x 1$-Alkanol + ( 1 - x) Dodecane\} at 298.15 K

|  | methanol | ethanol | 1-propanol | 1-butanol | 1-pentanol | 1-hexanol | 1-heptanol | 1-octanol | 1-nonanol | 1-decanol |  |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| $d_{j}$ |  |  |  |  |  |  |  |  |  |  |  |
| $d_{1}$ | 0.745421 | 0.745440 | 0.745439 | 0.745432 | 0.745427 | 0.745440 | 0.745434 | 0.745435 | 0.745417 | 0.745285 |  |
| $d_{2}$ | -0.011899 | -0.013325 | -0.004322 | 0.005512 | 0.015009 | 0.019818 | 0.029347 | 0.036440 | 0.045763 | 0.050725 |  |
| $d_{3}$ | 0.30395 | 0.42414 | 0.34415 | 0.22908 | 0.19099 | 0.35904 | 0.29561 | 0.35223 | 0.28678 | 0.39692 |  |
| $d_{4}$ | -3.2331 | -4.4955 | -2.9180 | -1.0625 | -0.8422 | -3.6430 | -2.6571 | -3.7304 | -2.7548 | -3.9688 |  |
| $d_{5}$ | 12.820 | 17.716 | 9.293 |  |  | 14.517 | 9.332 | 15.169 | 10.640 | 14.373 |  |
| $u_{\mathrm{d}} / \mathrm{g} \cdot \mathrm{cm}^{-3}$ | $2.6 \times 10^{-6}$ | $3.0 \times 10^{-6}$ | $1.2 \times 10^{-6}$ | $3.7 \times 10^{-6}$ | $6.2 \times 10^{-6}$ | $2.4 \times 10^{-6}$ | $2.3 \times 10^{-6}$ | $2.6 \times 10^{-6}$ | $4.9 \times 10^{-6}$ | $1.2 \times 10^{-6}$ |  |

was calibrated with an estimated standard deviation of $\pm 3 \times 10^{-6} \mathrm{~g} \cdot \mathrm{~cm}^{-3}$.

The mixtures used to measure density were prepared in specially designed vessels of $10 \mathrm{~cm}^{3}$ that avoid changes in $x$ caused by evaporation into the vapor phase above the liquid. ${ }^{5}$ The weights of sample liquids, the vapor phase, and the balance-weight were corrected against buoyancy.

The uncertainty in the mole fraction for the dilute region of alkanol ( $\delta x$ ) due to the uncertainty in weight is expressed with

$$
\begin{equation*}
\delta x=\left(M_{1} / M_{2}\right)\left(1 / w_{1}\right) \delta w_{2} \tag{1}
\end{equation*}
$$

where $M_{1}$ and $M_{2}$ are the molar masses of dodecane and

Table 4. Coefficients $\left(v_{j}\right)$ and Estimated Standard Uncertainty $\left(u_{v}\right)$ Determined by Eq 8 for $\{x 1$-Alkanol + ( $1-x$ )Dodecane $\}$ at 298.15 K



Figure 2. Observed apparent dipole moments of $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}(\mu)$ in dodecane at $298.15 \mathrm{~K}: \bullet, n=1 ; \bigcirc, n=2 ; \mathbf{\square}, n=3 ; \square, n=4$; $\mathbf{\Delta}, n=5 ; \Delta, n=6 ;, n=7 ; \diamond, n=8 ; \mathbf{\nabla}, n=9 ; \nabla, n=10 . \mu^{*}=$ $3.33564 \times 10^{-30} \mathrm{C} \cdot \mathrm{m}$. Lines are the least squares representation: (a) for $0<x<0.12$; (b) enlarged for $x<0.01$.

Figure 3. Dipole moments of isolated $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}\left(\mu_{0}\right)$ at 298.15 K. Our results: $O$, in dodecane; $\Delta$, in cyclohexane; ${ }^{4} \square$, in heptane. ${ }^{4}$ Literature values: + , in vapor phase; ${ }^{10} \mathbf{\nabla}$, in vapor phase; ${ }^{11}$, in vapor phase; ${ }^{12} \bullet$, in cyclohexane; ${ }^{9} \boldsymbol{\Delta}$, in cyclohexane; ${ }^{3}$ $■$, in cyclohexane. ${ }^{2} \mu^{*}=3.33564 \times 10^{-30} \mathrm{C} \cdot \mathrm{m}$.

1-alkanol, respectively, and $w_{1}$ and $w_{2}$ are the masses of dodecane and 1 -alkanol, respectively. By adopting the estimated standard uncertainty of 0.2 mg for $\delta w_{2}$ the uncertainty in $x$ reached the largest value of $1.4 \times 10^{-4}$ in the case of methanol + dodecane system.

The temperature for the measurements of $\rho$ was monitored with a thermometer (Precision Thermometry Bridge of Ninco Products, Inc., F300 MKII, England). It was calibrated with a triple-point water cell (home-made) and a Gallium cell (1740, Yellow Spring Instrument Co., USA). Thereby, the temperature was controlled at 298.15 K within an uncertainty of 0.01 K .

The excess molar volumes were calculated from density values as a function of $x$ by the relationship:

$$
\begin{equation*}
V_{\mathrm{m}}^{\mathrm{E}}=\left\{(1-x) M_{1}+x M_{2}\right\} / \rho-(1-x) M_{1} / \rho_{1}^{*}-x M_{2} / \rho_{2}^{*} \tag{2}
\end{equation*}
$$

where $\rho$ denotes the density of mixture; $\rho^{*}{ }_{1}$ and $\rho^{*}{ }_{2}$ are

Table 5. Relative Permittivities ( $\epsilon_{\mathrm{r}}$ ) and Apparent Dipole Moments of 1-Alkanols $\mu(F)$ Calculated by Eq 4 and $\mu(\mathrm{D})$ by Eq 6 at $298.15 \mathrm{~K}\left(\mu^{*}=3.33564 \times 10^{-30} \mathrm{C} \cdot \mathrm{m}\right)$

|  | $\epsilon_{\mathrm{r}}$ | $\mu(\mathrm{F}) / \mu^{*} \mu(\mathrm{D}) / \mu^{*}$ |  |  | $\epsilon_{\mathrm{r}}$ | $\mu(\mathrm{F}) / \mu^{*} \mu(\mathrm{D}) / \mu^{*}$ |  |  | $\epsilon_{\mathrm{r}}$ | $\mu(\mathrm{F}) / \mu^{*} \mu(\mathrm{D}) / \mu^{*}$ |  | $x$ |  | $\mu(\mathrm{F}) / \mu^{*} \mu(\mathrm{D}) / \mu^{*}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $x \mathrm{CH}_{3} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |  | $x \mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |  | $x \mathrm{C}_{3} \mathrm{H}_{7} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |  | $x \mathrm{C}_{4} \mathrm{H}_{9} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ |  |  |  |
| 0.000771 | 2.008222 | 1.667 | 1.648 | 0.000779 | 2.008124 | 1.643 | 1.639 | 0.001113 | 2.008412 | 1.613 | 1.619 | 0.000394 | 2.007748 | 1.599 | 1.612 |
| 0.001621 | 2.009272 | 1.666 | 1.646 | 0.001608 | 2.009152 | 1.644 | 1.640 | 0.001805 | 2.009261 | 1.612 | 1.619 | 0.001092 | 2.008608 | 1.596 | 1.608 |
| 0.002740 | 2.010659 | 1.665 | 1.646 | 0.002571 | 2.010350 | 1.645 | 1.640 | 0.002620 | 2.010262 | 1.611 | 1.618 | 0.001852 | 2.009553 | 1.598 | 1.610 |
| 0.003489 | 2.011589 | 1.664 | 1.645 | 0.003578 | 2.011599 | 1.644 | 1.639 | 0.003582 | 2.011456 | 1.613 | 1.619 | 0.002663 | 2.010557 | 1.597 | 1.609 |
| 0.004562 | 2.012925 | 1.664 | 1.645 | 0.004642 | 2.012927 | 1.644 | 1.639 | 0.004766 | 2.012923 | 1.613 | 1.619 | 0.003575 | 2.011694 | 1.598 | 1.610 |
| 0.005874 | 2.014482 | 1.655 | 1.636 | 0.005982 | 2.014531 | 1.636 | 1.631 | 0.006045 | 2.014492 | 1.611 | 1.617 | 0.004582 | 2.012951 | 1.598 | 1.610 |
| 0.008056 | 2.016939 | 1.635 | 1.615 | 0.007701 | 2.016532 | 1.624 | 1.620 | 0.007410 | 2.016128 | 1.606 | 1.611 | 0.005742 | 2.014384 | 1.596 | 1.608 |
| 0.010608 | 2.019513 | 1.602 | 1.583 | 0.009387 | 2.018400 | 1.610 | 1.605 | 0.009180 | 2.018154 | 1.594 | 1.599 | 0.007082 | 2.015999 | 1.591 | 1.602 |
| 0.013096 | 2.021872 | 1.573 | 1.554 | 0.011113 | 2.020222 | 1.594 | 1.589 | 0.011305 | 2.020401 | 1.573 | 1.578 | 0.008478 | 2.017621 | 1.582 | 1.593 |
| 0.014907 | 2.023498 | 1.554 | 1.535 | 0.013085 | 2.022090 | 1.569 | 1.564 | 0.014079 | 2.023126 | 1.545 | 1.550 | 0.009996 | 2.019302 | 1.569 | 1.581 |
| 0.018967 | 2.026970 | 1.515 | 1.497 | 0.015887 | 2.024614 | 1.538 | 1.533 | 0.018183 | 2.016847 | 1.505 | 1.510 | 0.011960 | 2.021339 | 1.550 | 1.561 |
| 0.02456 | 2.031548 | 1.475 | 1.457 | 0.02008 | 2.028153 | 1.498 | 1.493 | 0.02340 | 2.031194 | 1.462 | 1.466 | 0.014717 | 2.024049 | 1.523 | 1.534 |
| 0.03063 | 2.036439 | 1.444 | 1.425 | 0.02502 | 2.032142 | 1.461 | 1.456 | 0.02953 | 2.036123 | 1.423 | 1.427 | 0.01783 | 2.026932 | 1.495 | 1.506 |
| 0.03798 | 2.042625 | 1.423 | 1.404 | 0.03098 | 2.036888 | 1.428 | 1.423 | 0.03486 | 2.040329 | 1.398 | 1.401 | 0.02067 | 2.029389 | 1.471 | 1.481 |
| 0.04663 | 2.050229 | 1.409 | 1.390 | 0.03829 | 2.042741 | 1.401 | 1.395 | 0.04243 | 2.046346 | 1.371 | 1.374 | 0.02620 | 2.033992 | 1.432 | 1.441 |
| 0.05524 | 2.058340 | 1.405 | 1.385 | 0.04601 | 2.049071 | 1.381 | 1.375 | 0.05033 | 2.052715 | 1.352 | 1.355 | 0.03349 | 2.039841 | 1.392 | 1.401 |
| 0.06621 | 2.069539 | 1.408 | 1.388 | 0.05500 | 2.056819 | 1.369 | 1.362 | 0.06022 | 2.061082 | 1.338 | 1.340 | 0.04201 | 2.046631 | 1.360 | 1.368 |
| 0.08007 | 2.085608 | 1.425 | 1.403 | 0.06553 | 2.066488 | 1.363 | 1.356 | 0.07048 | 2.070192 | 1.330 | 1.332 | 0.05197 | 2.054660 | 1.335 | 1.343 |
|  |  |  |  | 0.07632 | 2.077165 | 1.365 | 1.357 | 0.08292 | 2.082062 | 1.329 | 1.329 | 0.06201 | 2.062984 | 1.319 | 1.326 |
|  |  |  |  | 0.08814 | 2.089857 | 1.372 | 1.363 | 0.09516 | 2.094737 | 1.333 | 1.333 | 0.07269 | 2.072278 | 1.310 | 1.316 |
|  |  |  |  | 0.10170 | 2.105961 | 1.385 | 1.375 | 0.10999 | 2.111571 | 1.345 | 1.343 | 0.08613 | 2.084755 | 1.306 | 1.311 |
|  |  |  |  |  |  |  |  |  |  |  |  | 0.09876 | 2.097321 | 1.308 | 1.313 |

$x \mathrm{C}_{5} \mathrm{H}_{11} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26} \quad x \mathrm{C}_{6} \mathrm{H}_{13} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26} \quad x \mathrm{C}_{7} \mathrm{H}_{15} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26} \quad x \mathrm{C}_{8} \mathrm{H}_{17} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}$ $\begin{array}{lllllllllllllll}0.000482 & 2.007671 & 1.590 & 1.607 & 0.000504 & 2.007990 & 1.577 & 1.598 & 0.000586 & 2.007864 & 1.577 & 1.600 & 0.000468 & 2.007818 & 1.561\end{array} 1.586$ $\begin{array}{llllllllllllllll}0.001089 & 2.008436 & 1.592 & 1.609 & 0.001087 & 2.008731 & 1.580 & 1.600 & 0.001199 & 2.008654 & 1.577 & 1.600 & 0.000994 & 2.008496 & 1.560 & 1.585\end{array}$ $1.608-0.0017952 .009633-1.582-1.602-0.0018731 .009525-1.577$ $0.0017962 .009241 .591 \quad 1.608 \quad 0.0017952 .009631 .582 \quad 1.6020 .0018731 .0095251 .5771 .600 \quad 0.0017402 .009581 .560$ 0.0025892 .0103181 .590 0.0034402 .0113961 .591 0.0045492 .0128041 .591 $0.005875 \quad 2.014478 \quad 1.590$ $0.0072952 .016230 \quad 1.586$ 0.0092162 .0184951 .574 0.0116222 .0211351 .552 0.0141012 .0236521 .528 $0.01688 \quad 2.0262851 .501$ $\begin{array}{lll}0.02110 & 2.030031 & 1.463\end{array}$ $\begin{array}{lll}0.02571 & 2.033879 & 1.428\end{array}$ $\begin{array}{lll}0.03208 & 2.039026 & 1.391\end{array}$ $0.03962 \quad 2.0449951 .357$ $\begin{array}{lll}0.04963 & 2.052978 & 1.327\end{array}$ $\begin{array}{lll}0.05931 & 2.060899 & 1.309\end{array}$ $\begin{array}{lll}0.07029 & 2.070108 & 1.295\end{array}$ $\begin{array}{lll}0.08177 & 2.080230 & 1.287\end{array}$ $\begin{array}{lll}0.09402 & 2.091619 & 1.284\end{array}$ $\begin{array}{llllllllllll}0.10681 & 2.104290 & 1.286 & 1.293 & 0.09410 & 2.091640 & 1.264 & 1.276 & 0.08135 & 2.080160 & 1.256\end{array}$ $\begin{array}{lllllllllllll}1.294 & 0.10523 & 2.102215 & 1.263 & 1.274 & 0.09339 & 2.090889 & 1.250 & 1.264 & 0.11105 & 2.107428 & 1.231 & 1.246\end{array}$ $\begin{array}{llll}0.10854 & 2.105048 & 1.248 & 1.261\end{array}$

$$
x \mathrm{C}_{10} \mathrm{H}_{21} \mathrm{OH}+(1-x) \mathrm{C}_{12} \mathrm{H}_{26}
$$

$\begin{array}{llllllllllllllllllll}0.000477 & 2.007822 & 1.558 & 1.585 & 0.02124 & 2.031180 & 1.420 & 1.443 & 0.001971 & 2.009738 & 1.554 & 1.583 & 0.01864 & 2.029002 & 1.444 & 1.470\end{array}$ $\begin{array}{llllllllllllllll}0.001008 & 2.008517 & 1.557 & 1.584 & 0.02410 & 2.033697 & 1.397 & 1.420 & 0.002902 & 2.010975 & 1.554 & 1.583 & 0.02121 & 2.031366 & 1.421 & 1.447\end{array}$ $\begin{array}{lllllllllllllll}0.001576 & 2.009265 & 1.557 & 1.585 & 0.02897 & 2.037840 & 1.364 & 1.387 & 0.003662 & 2.011985 & 1.554 & 1.582 & 0.02459 & 2.034256 & 1.392 \\ 1.417\end{array}$ $\begin{array}{llllllllllllllll}0.002254 & 2.010153 & 1.557 & 1.584 & 0.03592 & 2.043555 & 1.327 & 1.349 & 0.004525 & 2.013140 & 1.554 & 1.583 & 0.02958 & 2.038642 & 1.363 & 1.387\end{array}$ $\begin{array}{lllllllllll}0.002998 & 2.011122 & 1.554 & 1.581 & 0.04265 & 2.049022 & 1.301 & 1.321 & 0.005614 & 2.014591 & 1.554\end{array}$ $\begin{array}{lllllllllll}0.003815 & 2.012200 & 1.555 & 1.582 & 0.04937 & 2.054450 & 1.280 & 1.300 & 0.006788 & 2.016132 & 1.552\end{array}$ 0.0046392 .0132921 .556 0.0059852 .0150581 .555 0.0075532 .0170271 .546 $0.0095132 .019390 \quad 1.531$ 0.0123512 .0225531 .504 $\begin{array}{lll}0.01662 & 2.026872 & 1.461\end{array}$

| 1.583 | 0.05678 | 2.060471 | 1.263 | 1 |
| :--- | :--- | :--- | :--- | :--- | $1.2820 .0079832 .017642 \quad 1.545$ $\begin{array}{llll}1.267 & 0.009268 & 2.019198 & 1.535\end{array}$ $1.256 \quad 0.0108932 .021070 \quad 1.519$ $\begin{array}{llll}1.248 & 0.012832 & 2.023212 & 1.501\end{array}$ $1.241 \quad 0.014453 \quad 2.024922 \quad 1.485$

$\begin{array}{lllll}1.237 & 0.01654 & 2.027001 & 1.464 & 1.490\end{array}$
$\begin{array}{lllll}1.583 & 0.03739 & 2.045142 & 1.324 & 1.348 \\ 1.580 & 0.04685 & 2.052861 & 1.290 & 1.313\end{array}$ $\begin{array}{lllll}1.573 & 0.05669 & 2.060885 & 1.266 & 1.288\end{array}$ $\begin{array}{lllll}1.563 & 0.06704 & 2.069450 & 1.248 & 1.269\end{array}$ $\begin{array}{lllll}1.547 & 0.07856 & 2.079149 & 1.234 & 1.255\end{array}$ $\begin{array}{lllll}1.528 & 0.08846 & 2.087731 & 1.227 & 1.247\end{array}$ $\begin{array}{lllll}1.512 & 0.10509 & 2.102617 & 1.220 & 1.239\end{array}$
the densities of dodecane and 1-alkanol in pure state, respectively; and $M_{1}$ and $M_{2}$ are the molar masses of dodecane and 1-alkanol, respectively. The uncertainty in excess volume ( $\delta V_{\mathrm{m}}^{\mathrm{E}}$ ) was propagated from the uncertainty in the mole fraction $(\delta x)$ and that in the density of mixture $(\delta \rho)$. It was expressed for a region of $x<0.1$ by

$$
\begin{align*}
\delta V_{\mathrm{m}}^{\mathrm{E}}=M_{2}\left(1 / \rho_{1}^{*}-1 / \rho_{2}^{*}\right) & \delta x+ \\
& \left(1 / \rho^{2}\right)\left\{x M_{2}+(1-x) M_{1}\right\} \delta \rho \tag{3}
\end{align*}
$$

The uncertainty in the densities of pure liquid was negligible because relative values in density between the mixture and the component liquid determine the excess volumes. The deviation of $V_{\mathrm{m}}^{\mathrm{E}}$ propagated from the density of mixture ( $\delta \rho$ ) was about $9 \times 10^{-4} \mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}$ and that propagated from $\delta x$ was ( 3 to 6 ) $\times 10^{-4} \mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}$. Accordingly, the combined standard uncertainty in $V_{\mathrm{m}}^{\mathrm{E}}$ was estimated to be ( 9.5 to 10.9 ) $\times 10^{-4} \mathrm{~cm}^{3} \cdot \mathrm{~mol}^{-1}$.

The relative permittivities $\left(\epsilon_{\mathrm{r}}\right)$ were measured with a LCR meter (HP-4284A). A stepwise dilution method was

Table 6. Dipole Moments $\left(\mu_{0}\right)$ of $\mathrm{C}_{n} \mathrm{H}_{2 n+1} \mathrm{OH}$ at Infinite Dilution for $\boldsymbol{T}=\mathbf{2 9 8 . 1 5} \mathrm{K}$ Calculated by $\mathrm{Eq} 4\left(\mu^{*}=3.33564 \times 10^{-30}\right.$ C•m)

| $\mu_{0} / \mu^{*}$ |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | in dodecane | in heptane | in cyclohexane |  |  | in vapor |  |  |
| $n$ | present work | previous work ${ }^{a}$ | previous work ${ }^{\text {a }}$ | lit. | lit. | lit. | lit. | lit. |
| 1 | 1.666 | 1.666 | 1.664 |  |  | 1.69 f | $1.61{ }^{e}$ | $1.68{ }^{\text {e }}$ |
| 2 | 1.644 | 1.650 | 1.652 | $1.700^{\text {b }}$ |  | $1.67{ }^{\text {e }}$ |  |  |
| 3 | 1.613 | 1.627 | 1.629 | $1.630^{c}$ |  | $1.64{ }^{\text {g }}$ | $1.657^{e}$ |  |
| 4 | 1.598 | 1.612 | 1.614 | $1.623{ }^{\text {d }}$ | $1.615^{c}$ | $1.63{ }^{\text {e }}$ | $1.659{ }^{\text {e }}$ | $1.59{ }^{\text {g }}$ |
| 5 | 1.591 | 1.597 | 1.598 |  |  |  |  |  |
| 6 | 1.581 | 1.586 | 1.589 |  |  |  |  |  |
| 7 | 1.577 | 1.581 | 1.583 |  |  |  |  |  |
| 8 | 1.559 | 1.568 | 1.570 |  |  |  |  |  |
| 9 | 1.556 | 1.566 | 1.568 |  |  |  |  |  |
| 10 | 1.554 | 1.564 | 1.566 |  |  |  |  |  |

${ }^{a}$ Previous results reported in ref 4. ${ }^{b} \operatorname{Ref} 9 .{ }^{c} \operatorname{Ref} 3 .{ }^{d}$ Determined graphically from ref 2. ${ }^{e}$ Ref $10 . f$ Ref $11 .{ }^{g}$ Ref 12.
applied for fillings of the electrode cell with solution. The electrode cell, which consists of two cylindrical nickel plates, had a capacitance ( $C$ ) of 28 pF . The value of $C$ was measured with an repeatability of $\pm 0.0001 \mathrm{pF}$, which corresponded to an uncertainty of $\pm 3.5 \times 10^{-6}$ in $\epsilon_{\mathrm{r}}$. The Frohlich equation, ${ }^{6}$

$$
\begin{gather*}
V_{\mathrm{m}}\left(\epsilon_{\mathrm{r}}-1\right) / 3 \epsilon_{\mathrm{r}}=(1-x) V^{*}{ }_{1}\left(\epsilon_{\mathrm{r}, 1}^{*}-1\right) /\left(\epsilon_{\mathrm{r}, 1}^{*}+2 \epsilon_{\mathrm{r}}\right)+ \\
x V_{2}^{*}\left(\epsilon_{\mathrm{r}, 2}{ }^{\prime}-1\right) /\left(\epsilon_{\mathrm{r}, 2}{ }^{\prime}+2 \epsilon_{\mathrm{r}}\right)+ \\
4 \pi N_{\mathrm{A}} x g \mu_{0}^{2}\left(\epsilon_{\mathrm{r}, 2}^{\prime}+2\right)^{2}\left(2 \epsilon_{\mathrm{r}}+1\right) / 27 k T\left(\epsilon_{\mathrm{r}, 2}{ }^{\prime}+2 \epsilon_{\mathrm{r}}\right)^{2} \tag{4}
\end{gather*}
$$

was used to calculate $\mu$ values. It is expressed in terms of relative permittivity for the solution, $\epsilon_{\mathrm{r}}$, that for dodecane, $\epsilon_{\mathrm{r}, 1}$, the molar volume of the solution, $V_{\mathrm{m}}$, the molar volume of dodecane, $V^{*}{ }_{1}$, the molar volume of 1-alkanol, $V^{*}{ }_{2}$, and the "internal permittivity" of 1-alkanol, $\epsilon_{\mathrm{r}, 2}{ }^{\prime}$ activated by infrared radiation. Here, $N_{\mathrm{A}}$ is Avogadro constant, $k$ is Boltzmann constant, and $g$ is the "Kirkwood $g$-factor". ${ }^{7}$ The apparent dipole moment ( $\mu$ ) is defined as $\mu$ $=\left(g \mu^{2}\right)^{1 / 2}$. We calculated $\epsilon_{\mathrm{r}, 2}{ }^{\prime}$ from the Clausius - Mossotti equation, adopting the atomic polarization $\left(P_{\mathrm{A}}\right)$ that was evaluated using the assumed relation:

$$
\begin{equation*}
P_{\mathrm{E}}+P_{\mathrm{A}}=1.10 P_{\mathrm{E}} \tag{5}
\end{equation*}
$$

where $P_{\mathrm{E}}$ was calculated by the Lorenz-Lorentz equation using the refractive index for the sodium-D line, $n_{\mathrm{D}}$. We also calculated $\mu$ values by Debye equation:

$$
\begin{array}{r}
V_{\mathrm{m}}\left(\epsilon_{\mathrm{r}}-1\right) /\left(\epsilon_{\mathrm{r}}+2\right)=(1-x) V_{1}^{*}\left(\epsilon_{\mathrm{r}, 1}^{*}-1\right) /\left(\epsilon_{\mathrm{r}, 1}^{*}+2\right)+ \\
x V_{2}^{*}\left(\epsilon_{\mathrm{r}}-1\right) /\left(\epsilon_{\mathrm{r}}+2\right)+4 \pi N_{\mathrm{A}} x \mu_{0}^{2} / 9 k T \tag{6}
\end{array}
$$

We used the same equations for eqs 4 to 6 as those used by French et al. ${ }^{2}$ so that the experimental results can be compared based on the same method of calculation.

The expanded uncertainty in $\mu_{0}$ (with a coverage factor, $k=2$ ) was estimated to be 0.002 D by means of simulations adopting the uncertainty in $\epsilon_{\mathrm{r}}$ to eq 4 , where $\mathrm{D}=3.33564$ $\times 10^{-30} \mathrm{C} \cdot \mathrm{m}$. The experimental techniques for $V_{\mathrm{m}}^{\mathrm{E}}$ and $\mu$ measurements have been described in detail in the previous reports. ${ }^{3,4}$

## Results and Discussion

Excess Volume. The values of $\rho$ and $V_{\mathrm{m}}^{\mathbb{E}}$ are listed in Table 2. The function

$$
\begin{equation*}
\rho /\left(\mathrm{g} \cdot \mathrm{~cm}^{-3}\right)=\sum d_{j} x^{(j-1)} \tag{7}
\end{equation*}
$$

was fitted to each set of densities, and the smoothing function

$$
\begin{equation*}
V_{\mathrm{m}}^{\mathrm{E}} /\left(\mathrm{cm}^{3} \cdot \mathrm{~mol}^{-1}\right)=x(1-x) \sum v_{j} x^{(j-1)} \tag{8}
\end{equation*}
$$

was fitted to excess volumes by the least-squares method. The values of coefficients $\left(d_{j}\right)$ and the estimated standard uncertainties $\left(u_{\mathrm{d}}\right)$ determined for eq 7 are summarized in Table 3. The coefficients of $v_{i}$ are listed in Table 4 with the estimated standard uncertainty, $u_{\mathrm{v}}$. In Figure 1, the excess partial molar volumes of 1-alkanol at the infinite dilution $\left(V_{2}^{\mathrm{E}, \infty}\right)$, the numerical value of which equals to $v_{1}$ of eq 8 , are plotted along with our previous results for 1 -alkanols determined in cyclohexane and heptane and also with literature values measured in alkanes at 298.15 K . The limiting value ( $V_{2}^{\mathrm{E}, \infty}$ ) is defined by

$$
\begin{equation*}
V_{2}^{\mathrm{E}, \infty}=V_{2}^{\infty}-V_{2}^{*} \tag{9}
\end{equation*}
$$

where $V_{2}^{\infty}$ and $V_{2}{ }^{*}$ are the partial molar volumes of alkanol at infinite dilution and in pure state, respectively. Therefore, $V_{2}^{\mathrm{E}, \infty}$ denotes the change in partial molar volume of alkanol performed by the transfer between the two media of pure alkanol and an alkane. The uncertainty at the vicinity of the infinite dilution varied depending on the system, and it was estimated to be less than $\pm 0.9$ $\mathrm{cm}^{3} \cdot \mathrm{~mol}^{-1}$. For all the alkanols the values of $V_{2}^{\mathrm{E}, \infty}$ in cyclohexane were the same within the experimental uncertainty. On the other hand, $V_{2}^{\mathrm{E}, \infty}$ in $n$-alkane decreased systematically with increasing chain length of 1 -alkanol. The value of methanol was constant, irrespective of solvent, and it was $(7.6 \pm 0.7) \mathrm{cm}^{3} \cdot \mathrm{~mol}^{-1}$.
Apparent Dipole Moment. To investigate the dielectric relaxation we measured the relative permittivities for 1-butanol + cyclohexane at frequencies of 20,30 , and 100 kHz . The calculated values of $\mu$ at these frequencies agreed within 0.001 D over the observed mole fraction. Therefore, we concluded that the dielectric loss is negligible at the frequency lower than 100 kHz . We employed the capacitances measured at the frequency of 30 kHz because the $C$ value fluctuated due to the metal stirrer placed in the oil bath at a frequency lower than 20 kHz . The experimental results for $\epsilon_{\mathrm{r}}$ and $\mu$ calculated by the Frohlich and Debye equations are listed in Table 5. Frohlich equation gave a larger value for $\mu_{0}$ of methanol and ethanol than that calculated by Debye equation, whereas Debye equation gave larger values as the chain length of alkanol increased. A maximum difference, viz., 0.03 D , occurred for 1-decanol. The Frohlich equation is based on the cavity
field and the reaction field proposed by Onsager. ${ }^{8}$ The difference found in the calculated $\mu$ values resulted from these two equations were discussed from a viewpoint of the reaction field in the previous publications. ${ }^{4,9}$

The $\mu$ values determined by Frohlich equation are represented in Figure 2, where the curves are least squares representations. An enlarged plots for a region of $x<0.01$ is shown in Figure 2b. The value of $\mu$ was constant in the region of $x<0.006$ for each alkanol and decreased sharply due to the onset of intermolecular association of alkanols. These aspects have been commonly observed in binary systems consist of alkanol and nonpolar solvent. ${ }^{2-4,9}$ The dipole moments of isolated alkanols $\left(\mu_{0}\right)$ were determined by taking an average for the points that had a constant value independent of $x$.

The present results for $\mu_{0}$ calculated by Frohlich equation are listed in Table 6 with literature values. Here the values measured in vapor phase were calculated by the Debye equation, and our previous results determined in cyclohexane and heptane were determined by the Frohlich equation. Those values of $\mu_{0}$ are plotted in Figure 3.

The observed values of $\mu_{0}$ for methanol were the same within $\pm 0.001 \mathrm{D}$, irrespective of the three tested solvents, whereas it decreased with increasing chain-length of 1-alkanol. Small but systematic changes in $\mu_{0}$ due to solvent were observed for each alkanol except for methanol. The magnitude of $\mu_{0}$ of each alkanol was largest in cyclohexane and decreased in straight-chain hydrocarbons. The value in dodecane was smaller than that in heptane exceeding the uncertainty of determination. We found that the dipole moment of 1-alkanol varies with the relative direction of the group moment of - OH and the terminal group of $-\mathrm{CH}_{3}$ by means of ab initio calculations. ${ }^{4}$ The present experimental results imply that the rotation of the segments in alkanol is restricted in a solvent of straight and long-chain hydrocarbon due to the dispersion force that acts between the hydrocarbons of solute and solvent molecules. A restricted rotation of the segments of alkanols in a longchain alkane would reveal this behavior.

Marsh and co-workers determined the dipole moments of 1-alkanols in various solvents at different temperatures by means of the Frohlich equation. ${ }^{2,9}$ Our values for 1-butanol in cyclohexane agreed with their value with a difference less than 0.01 D . The determinations in vapor phase have been carried out based on the Debye equation assuming independence of temperature over a range of 100 K . The values in vapor phase reported by Wesson, ${ }^{10}$ Ramswamy, ${ }^{11}$ and Kubo ${ }^{12}$ showed considerable discrepancies. We did not find the values of 1 -alkanols for $n \geq 5$ measured in vapor phase.

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